

(OR)

- Construct the relationship between the pack **(b)** column with respect to gas and liquid phase ma
- Derive Rayleigh's equation with diffe (i) 12. (a) setup.
 - Analyze the effect of Reflux ratio on co (ii) (OR)
 - Analyze about the McCabe-Thiele met **(b)** (i) obtaining theoretical plates including assi and Limitations.
 - (ii) Analyze the q value for various thermal c diagram.
- 1000 kg/hr of an acetone-water mixture co 13. (a) acetone is to be counter-currently extracted recovered solvent to be used is free from trichloroethane are insoluble. If 90% reco estimate the number of stages required if 1.5 used. The equilibrium relationship is given by weight fractions of acetone in water and trichle (OR)
 - Write the procedure to calculate the number **(b)** Multi-stage Liquid-Liquid extraction process.
- 14. (a)

Oil is to be extracted from meal by means of counter current extraction unit. The unit is e meal (based on completely exhausted solid) contains 365 kg of oil and 30 kg of benzene. kg of oil and 590 kg of benzene. The exhaust of unextracted oil. The experimental data on meal by means of benzene at a given operating

			-	
Solution	composition,	kg	oil/kg	Solution
solution				underflo
				Kg solut
0				0.500
0.1				0.505
0.2				0.515
0.3				0.530
0.4				0.550
05				0.571
0.6				0.595
0.7				0.620

isothermal. The equilibrium relation is given by y = 0.76 x, where y, x are gas and liquid phase composition of ammonia in mole fraction respectively.

The overall mass transfer coefficient is 1.1 kg mole/m³ atm.min

) ted height of the absorption ass transfer co-efficient.	(14)	1	5
erential distillation diagram	(9)	2	4
ost.	(5)	2	4
) hod with graphical steps for umptions, stepwise procedure	(9)	2	4
conditions with a neat	(5)	2	4
ontaining 20% by weight of d with trichloroethane. The m acetone. The water and overy of acetone is desired times the minimum solvent is y = 1.65x, where x and y are procethane respectively.	(14)	3	3
) of stages for counter current	(14)	3	3
f benzene using a continuous expected to treat 1000 kg of per hour. The untreated meal The solvent used contains 14 ed solids are to contain 55 kg the extraction of oil from the g temperature are as follows retained (in w) ion/kg solids	(14)	4	5

Determine the number of ideal stages required.

(**OR**)

By extraction with kerosene two tones of waxed paper per day is to be (14) **(b)** dewaxed in a continuous countercurrent extraction system. The waxed paper contains 25% paraffin wax by weight and 75% paper pulp. The pulp which retains the unextracted wax must not contain over 0.2 kg of wax/100 kg of wax free pulp. The kerosene used for extraction contains 0.05 kg of wax/100 kg of wax free kerosene, experiments show that pulp retains 2 kg of kerosene per kg of wax free pulp. The extract from battery contains 5 kg of wax/100 kg of wax free kerosene. Determine the number of stages needed.

15. (a) A solid adsorbent is used to remove colour impurity from an aqueous solution. The original value of colour on an arbitrary scale is 48. It is required to reduce this to 10% of its original value. Using the following data, find the quantity of fresh adsorbent used for 1500 kg of solution for (7) (a) a single stage and (7)

(b) a two-stage cross current operation

when the intermediate colour value is 24.

Kg adsorbent of solution	0	0.001	0005	0.008	0.03	0.06
Equilibrium colour (y)	48	41	30	20	10.5	3.5

(OR)

(i) Analyze the principles of ion exchange techniques and its (7) 5 **(b)** 4 applications. (ii) Write about various membrane techniques available for desalination (7) 5 4 process.

PART- C(1x 10=10Marks)

(Q.No.16 is compulsory)

Marks CO RBT LEVEL

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Discuss the applications of absorption process in the abatement of pollution 16. (10) 1 in Chemical Process industries.

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